



**Exergoeconomic performance optimization of an  
endoreversible intercooled regenerated Brayton  
cogeneration plant  
Part 2: Heat conductance allocation and pressure ratio  
optimization**

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**Abstract**

Finite time exergoeconomic performance of an endoreversible intercooled regenerative Brayton cogeneration plant is optimized based on the model which is established using finite time thermodynamic in Part 1 of this paper. It is found that the optimal heat conductance allocation of the regenerator is zero. When the total pressure ratio and the heat conductance allocation of the regenerator are fixed, it is shown that there exist an optimal intercooling pressure ratio, and a group of optimal heat conductance allocations among the hot-, cold- and consumer-side heat exchangers and the intercooler, which correspond to a maximum dimensionless profit rate. When the total pressure ratio is variable, there exists an optimal total pressure ratio which corresponds to a double-maximum dimensionless profit rate, and the corresponding exergetic efficiency is obtained. The effects of the total heat exchanger conductance, price ratios and the consumer-side temperature on the double-maximum dimensionless profit rate and the corresponding exergetic efficiency are discussed. It is found that there exists an optimal consumer-side temperature which corresponds to a thrice-maximum dimensionless profit rate.

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**Keywords:** Endoreversible intercooled regenerative Brayton cogeneration plant, Profit rate, Exergetic efficiency, Finite time thermodynamics, Heat conductance allocation, Pressure ratio, Optimization.

**1. Introduction**

A thermodynamic model of an endoreversible intercooled regenerative Brayton cogeneration plant is established using finite time thermodynamic in Part 1 [1] of this paper based on the Refs. [2-8]. The analytical formulae about the relations among the dimensionless profit rate, exergetic efficiency and the effectivenesses of the five heat exchangers, the intercooling pressure ratio and the total pressure ratio are derived. The dimensionless profit rate will be optimized by using the similar principle and method used in various intercooled regenerative Brayton cycles [9-17] in which the power, efficiency and power density were taken as the optimization objectives, respectively.

The exergoeconomic performance optimization is performed by searching the optimal intercooling pressure ratio and the optimal heat conductance allocations among the hot-, cold- and consumer-side heat

exchangers, the intercooler and the regenerator for the fixed total pressure ratio. When the total pressure ratio is variable, the performance optimization is performed further by searching the optimal total pressure ratio. The effects of the ratio of the hot-side heat reservoir temperature to environment temperature, the total heat exchanger conductance, price ratios and the consumer-side temperature parameter on the exergoeconomic performance are studied.

**2. Numerical examples**

According to equation (19) in Part 1 of this paper, the dimensionless profit rate ( $\bar{\Pi}$ ) of the endoreversible intercooled regenerative Brayton cogeneration plant coupled to constant- temperature heat reservoirs is the function of the intercooling pressure ratio ( $\pi_1$ ), the total pressure ratio ( $\pi$ ) and the five heat conductances ( $U_H, U_L, U_K, U_I, U_R$ ) when the other boundary condition parameters ( $T_H, T_L, T_I, T_K, C_{wrf}$ ) are fixed. Equation (19) includes the optimal results of some Brayton cogeneration cycles. When  $U_R = 0$ , one can obtain the results of an endoreversible intercooled Brayton cogeneration cycle. When  $U_I = 0$ , one can obtain the results of an endoreversible regenerated Brayton cogeneration cycle [8]. When  $U_R = 0$  and  $U_I = 0$ , one can obtain the results of an endoreversible simple Brayton cogeneration cycle [7].

In practical design,  $\pi_1, \pi, U_H, U_L, U_K, U_I, U_R$  are changeable and the cost per unit of heat conductance may be different for each heat exchanger because different materials may be used. To simplify the problem, the constraint on total heat exchanger conductance is used for the performance optimization. Assuming that the total heat exchanger conductance ( $U_T = U_H + U_L + U_K + U_I + U_R$ ) is fixed, a group of heat conductance allocations are defined as:

$$u_h = U_H / U_T, u_l = U_L / U_T, u_k = U_K / U_T, u_i = U_I / U_T, u_r = U_R / U_T \tag{1}$$

Additionally, one has the constraints:

$$0 < u_h < 1, 0 < u_l < 1, 0 < u_k < 1, 0 < u_i < 1, 0 < u_r < 1, u_h + u_l + u_k + u_i + u_r = 1 \tag{2}$$

For the fixed  $\pi$  and  $\pi_1$ , the optimization can be performed by searching the optimal heat conductance allocations ( $(u_h)_{\bar{\Pi}_{opt}}, (u_l)_{\bar{\Pi}_{opt}}, (u_k)_{\bar{\Pi}_{opt}}, (u_i)_{\bar{\Pi}_{opt}}, (u_r)_{\bar{\Pi}_{opt}}$ ) which lead to an optimal dimensionless profit rate ( $\bar{\Pi}_{opt}$ ). One can always obtain  $(u_r)_{\bar{\Pi}_{opt}} = 0$ . The reason is that for the Brayton cycle discussed herein, the regeneration has little effect on the optimal dimensionless profit rate.

Another method is adopted herein: when  $u_r$  and  $\pi$  are fixed, the optimization can be performed by searching the other four optimal heat conductance allocations ( $(u_h)_{\bar{\Pi}_{max}}, (u_l)_{\bar{\Pi}_{max}}, (u_k)_{\bar{\Pi}_{max}}, (u_i)_{\bar{\Pi}_{max}}$ ) and the optimal intercooling pressure ratio ( $(\pi_1)_{\bar{\Pi}_{max}}$ ) which lead to a maximum dimensionless profit rate ( $\bar{\Pi}_{max}$ ).

To search the optimal values of  $u_h, u_l, u_k, u_i$  and  $\pi_1$ , the numerical calculations are provided by using the optimization toolbox of Matlab 7.1. In the calculations, four temperature ratios are defined:  $\tau_1 = T_H / T_0, \tau_2 = T_L / T_0, \tau_3 = T_I / T_0$  and  $\tau_4 = T_K / T_0$ , and  $U_T = 10kW / K, u_r = 0.1, k = 1.4, C_{wrf} = 1.0kW / K, \tau_2 = \tau_3 = 1, \tau_4 = 1.2$  are set. According to analysis in Ref. [18],  $a = 10$  and  $b = 6$  are set.

*2.1 Optimal dimensionless profit rate and corresponding exergetic efficiency*

Assuming that  $\pi = 18 (1 \leq \pi_1 \leq 18)$ . Figure 1 shows the characteristic of the optimal dimensionless profit rate ( $\bar{\Pi}_{opt}$ ) versus  $\pi_1$  for different  $\tau_1$ . Figure 2 shows the characteristics of the optimal heat conductance allocations ( $(u_j)_{\bar{\Pi}_{opt}}, j=h,l,k,i$ ) and the corresponding exergetic efficiency ( $(\eta_{ex})_{\bar{\Pi}_{opt}}$ ) versus  $\pi_1$  with  $\tau_1 = 5.0$ .

It can be seen from Figure 1 that  $\bar{\Pi}_{opt}$  increases with the increase of  $\pi_1$ . There exists an optimal value of intercooling pressure ratio ( $(\pi_1)_{\bar{\Pi}_{max}}$ ) which leads to a maximum dimensionless profit rate ( $\bar{\Pi}_{max}$ ). The calculation illustrates that when  $\pi_1$  is increased to a certain value, one has  $(u_i)_{\bar{\Pi}_{opt}} = 0$ . It can be seen from Figure 2 that with the increase of  $\pi_1, (u_h)_{\bar{\Pi}_{opt}}$  and  $(u_k)_{\bar{\Pi}_{opt}}$  decrease first and then increase,  $(u_l)_{\bar{\Pi}_{opt}}$

increases and  $(u_i)_{\bar{\Pi}_{opt}}$  decreases except that  $\pi_1$  is very small. The optimal heat conductance allocations which correspond to  $\bar{\Pi}_{max}$  are  $(u_j)_{\bar{\Pi}_{max}, j=h,l,k,i} \cdot (\eta_{ex})_{\bar{\Pi}_{opt}}$  exists a maximum value and a minimum value, and the exergetic efficiency corresponding to  $\bar{\Pi}_{max}$  is  $(\eta_{ex})_{\bar{\Pi}_{max}}$ .

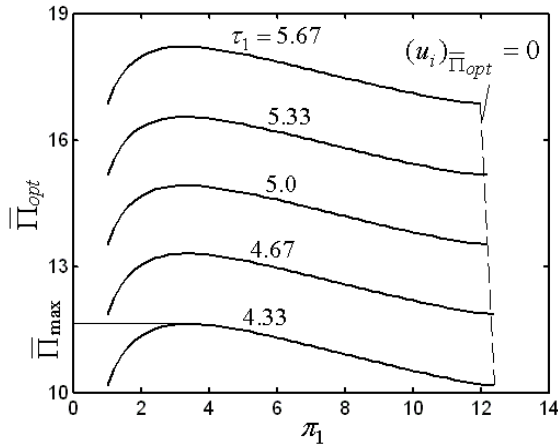


Figure 1. Effect of  $\tau_1$  on the characteristic of  $(\bar{e}_{out})_{opt}$  versus  $\pi_1$

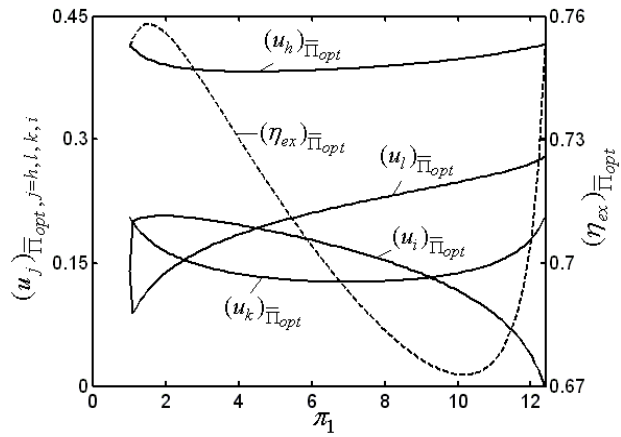


Figure 2. Characteristic of  $(u_j)_{\bar{\Pi}_{opt}, j=h,l,k,i}$  and  $(\eta_{ex})_{\bar{\Pi}_{opt}}$  versus  $\pi_1$

2.2 Maximum dimensionless profit rate and corresponding exergetic efficiency

Figures 3 and 4 show the characteristics of the maximum dimensionless profit rate ( $\bar{\Pi}_{max}$ ) and the corresponding exergetic efficiency  $(\eta_{ex})_{\bar{\Pi}_{max}}$ , the optimal heat conductance allocations  $(u_j)_{\bar{\Pi}_{max}, j=h,l,k,i}$  and optimal intercooling pressure ratio  $(\pi_1)_{\bar{\Pi}_{max}}$  versus  $\pi$  with  $\tau_1 = 5.0$ , respectively. It can be seen from Figure 3 that there exists an optimal value of total pressure ratio ( $\pi_{\bar{\Pi}_{max,2}}$ ) which lead to a double-maximum dimensionless profit rate ( $\bar{\Pi}_{max,2}$ ), and  $\bar{\Pi}_{max}$  changes slowly when  $\pi$  is large.  $(\eta_{ex})_{\bar{\Pi}_{max}}$  exists an extremum with respect to  $\pi$ , and the exergetic efficiency corresponding to  $\bar{\Pi}_{max,2}$  is  $(\eta_{ex})_{\bar{\Pi}_{max,2}}$ . It can be seen from Figure 4 that with the increase of  $\pi$ ,  $(u_h)_{\bar{\Pi}_{max}}$  and  $(u_k)_{\bar{\Pi}_{max}}$  decrease,  $(u_i)_{\bar{\Pi}_{max}}$ ,  $(u_l)_{\bar{\Pi}_{max}}$  and  $(\pi_1)_{\bar{\Pi}_{max}}$  increase. The optimal heat conductance allocations corresponding to  $\bar{\Pi}_{max,2}$  are  $(u_j)_{\bar{\Pi}_{max,2}, j=h,l,k,i}$ .

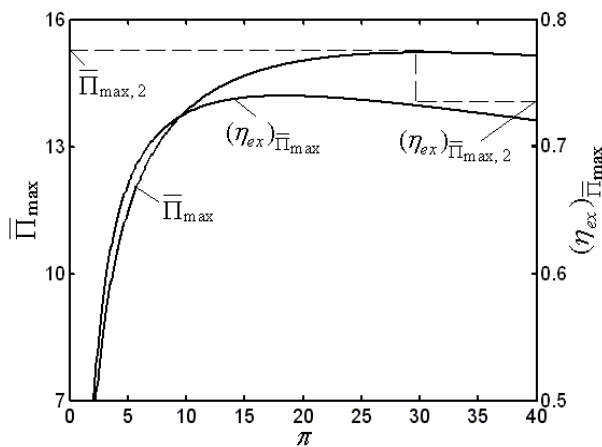


Figure 3. Characteristics of  $\bar{\Pi}_{max}$  and  $(\eta_{ex})_{\bar{\Pi}_{max}}$  versus  $\pi$

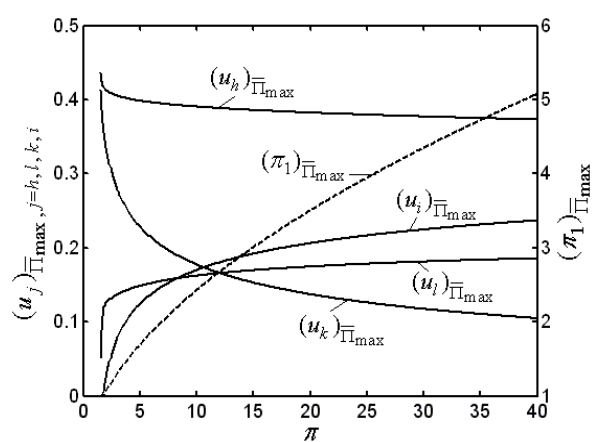


Figure 4. Characteristics of  $(u_j)_{\bar{\Pi}_{max}, j=h,l,k,i}$  and  $(\pi_1)_{\bar{\Pi}_{max}}$  versus  $\pi$

**3. Effects of total heat conductance, price ratios and consumer-side temperature**

Figures 5 and 6 show the characteristics of the double-maximum dimensionless profit rate ( $\bar{\Pi}_{\max, 2}$ ) and the corresponding exergetic efficiency ( $(\eta_{ex})_{\bar{\Pi}_{\max, 2}}$ ), the optimal heat conductance allocations ( $(u_j)_{\bar{\Pi}_{\max, 2}, j=h, l, k, i}$ ) and the optimal total pressure ratio ( $\pi_{\bar{\Pi}_{\max, 2}}$ ) versus  $U_T$  with  $\tau_1 = 5.0$ , respectively. It can be seen from Figure 5 that  $\bar{\Pi}_{\max, 2}$  and  $(\eta_{ex})_{\bar{\Pi}_{\max, 2}}$  increase with the increase of  $U_T$ , and increase slowly when  $U_T$  is large. It can be seen from Figure 6 that with the increase of  $U_T$ ,  $(u_h)_{\bar{\Pi}_{\max, 2}}$  decreases,  $(u_i)_{\bar{\Pi}_{\max, 2}}$  and  $\pi_{\bar{\Pi}_{\max, 2}}$  increase, and  $(u_l)_{\bar{\Pi}_{\max, 2}}$  and  $(u_k)_{\bar{\Pi}_{\max, 2}}$  decrease first and then increase.

Figures 7 and 8 show the characteristics of  $\bar{\Pi}_{\max, 2}$  and  $(\eta_{ex})_{\bar{\Pi}_{\max, 2}}$ ,  $(u_j)_{\bar{\Pi}_{\max, 2}, j=h, l, k, i}$  and  $\pi_{\bar{\Pi}_{\max, 2}}$  versus price ratio ( $a$ ), respectively. It can be seen from Figure 7 that with the increase of  $a$ ,  $\bar{\Pi}_{\max, 2}$  increases, and  $(\eta_{ex})_{\bar{\Pi}_{\max, 2}}$  increases first and then decreases. It can be seen from Figure 8 that with the increase of  $a$ ,  $(u_h)_{\bar{\Pi}_{\max, 2}}$  changes slightly,  $(u_k)_{\bar{\Pi}_{\max, 2}}$  decreases, and  $(u_i)_{\bar{\Pi}_{\max, 2}}$ ,  $(u_l)_{\bar{\Pi}_{\max, 2}}$ , and  $\pi_{\bar{\Pi}_{\max, 2}}$  increase.

Figures 9 and 10 show the characteristics of  $\bar{\Pi}_{\max, 2}$  and  $(\eta_{ex})_{\bar{\Pi}_{\max, 2}}$ ,  $(u_j)_{\bar{\Pi}_{\max, 2}, j=h, l, k, i}$  and  $\pi_{\bar{\Pi}_{\max, 2}}$  versus price ratio ( $b$ ), respectively. It can be seen from Figure 9 that  $\bar{\Pi}_{\max, 2}$  and  $(\eta_{ex})_{\bar{\Pi}_{\max, 2}}$  increase with the increase of  $b$ . It can be seen from Figure 10 that with the increase of  $b$ ,  $(u_h)_{\bar{\Pi}_{\max, 2}}$  changes slightly,  $(u_k)_{\bar{\Pi}_{\max, 2}}$  increases,  $(u_l)_{\bar{\Pi}_{\max, 2}}$  decreases, and  $(u_i)_{\bar{\Pi}_{\max, 2}}$  and  $\pi_{\bar{\Pi}_{\max, 2}}$  decrease approximately linearly.

Figures 11 and 12 show the characteristics of  $\bar{\Pi}_{\max, 2}$  and  $(\eta_{ex})_{\bar{\Pi}_{\max, 2}}$ ,  $(u_j)_{\bar{\Pi}_{\max, 2}, j=h, l, k, i}$  and  $\pi_{\bar{\Pi}_{\max, 2}}$  versus  $\tau_4$ , respectively. It can be seen from Figure 11 that there exists an optimal consumer-side temperature which leads to a thrice-maximum dimensionless profit rate.  $(\eta_{ex})_{\bar{\Pi}_{\max, 2}}$  also exists an extremum with respect to  $\tau_4$ . It can be seen from Figure 12 that with the increase of  $\tau_4$ ,  $(u_h)_{\bar{\Pi}_{\max, 2}}$  changes slightly,  $(u_k)_{\bar{\Pi}_{\max, 2}}$  decreases,  $(u_l)_{\bar{\Pi}_{\max, 2}}$  increases, and  $(u_i)_{\bar{\Pi}_{\max, 2}}$  and  $\pi_{\bar{\Pi}_{\max, 2}}$  decrease first and then increase.

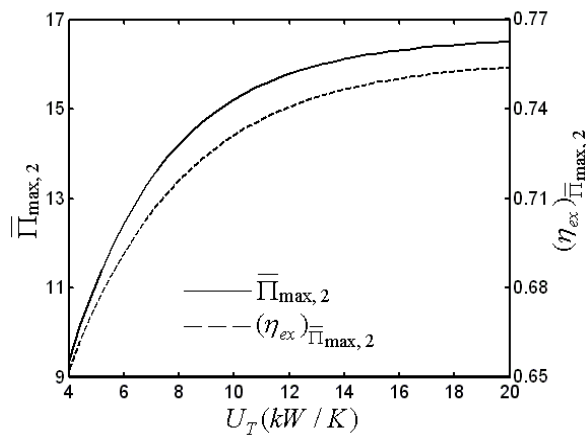


Figure 5. Characteristics of  $\bar{\Pi}_{\max, 2}$  and  $(\eta_{ex})_{\bar{\Pi}_{\max, 2}}$  versus  $U_T$

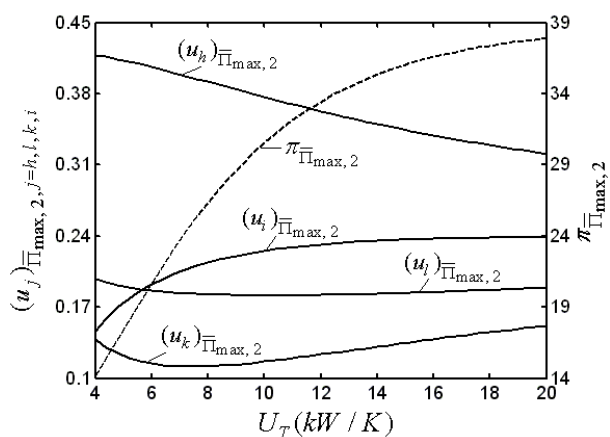


Figure 6. Characteristics of  $(u_j)_{\bar{\Pi}_{\max, 2}, j=h, l, k, i}$  and  $\pi_{\bar{\Pi}_{\max, 2}}$  versus  $U_T$

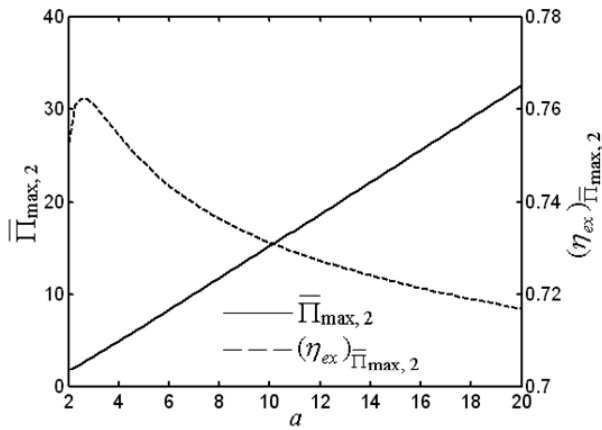


Figure 7. Characteristics of  $\bar{\Pi}_{max,2}$  and  $(\eta_{ex})_{\bar{\Pi}_{max,2}}$  versus  $a$

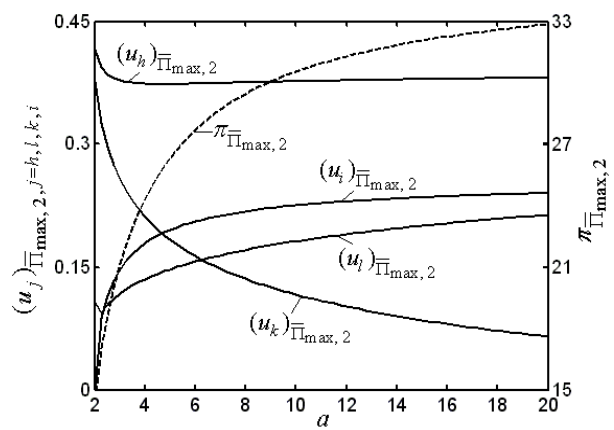


Figure 8. Characteristics of  $(u_j)_{\bar{\Pi}_{max,2}}$ ,  $j=h, l, k, i$  and  $\pi_{\bar{\Pi}_{max,2}}$  versus  $a$

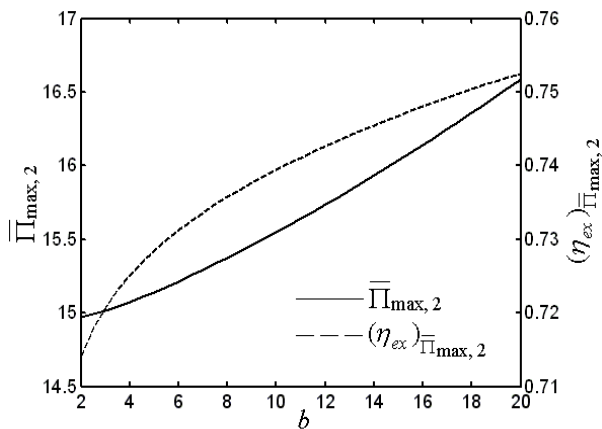


Figure 9. Characteristics of  $\bar{\Pi}_{max,2}$  and  $(\eta_{ex})_{\bar{\Pi}_{max,2}}$  versus  $b$

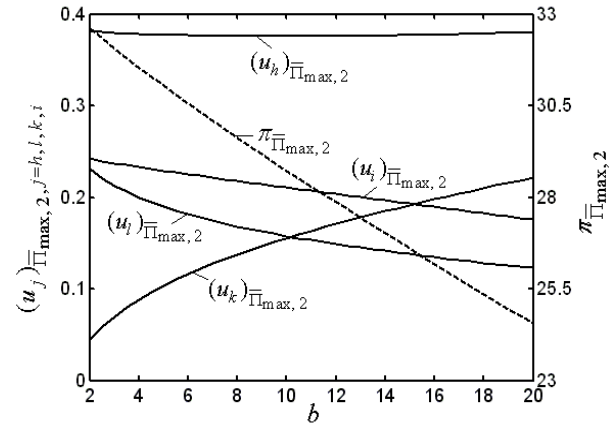


Figure 10. Characteristics of  $(u_j)_{\bar{\Pi}_{max,2}}$ ,  $j=h, l, k, i$  and  $\pi_{\bar{\Pi}_{max,2}}$  versus  $b$

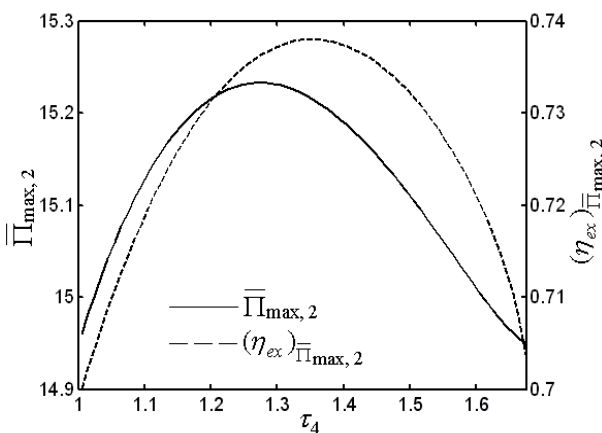


Figure 11. Characteristics of  $\bar{\Pi}_{max,2}$  and  $(\eta_{ex})_{\bar{\Pi}_{max,2}}$  versus  $\tau_4$

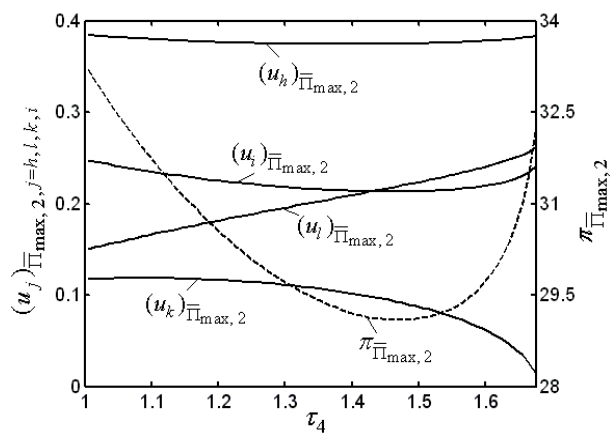


Figure 12. Characteristics of  $(u_j)_{\bar{\Pi}_{max,2}}$ ,  $j=h, l, k, i$  and  $\pi_{\bar{\Pi}_{max,2}}$  versus  $\tau_4$

#### 4. Conclusion

Finite time exergoeconomic performance of a heat and power cogeneration plant model composed of an endoreversible intercooled regenerative Brayton closed-cycle coupled to constant-temperature heat reservoirs is optimized by numerical examples. The main conclusions are as follows:

(1) When the optimization is performed with respect to the five heat conductance allocations of the hot-, cold- and consumer-side heat exchangers, the intercooler and the regenerator for a fixed total heat exchanger conductance, the optimal heat conductance allocation of the regenerator is always zero in the operation state of optimal dimensionless profit rate.

(2) When the heat conductance allocation of the regenerator and the total pressure ratio are fixed, there exist an optimal intercooling pressure ratio and a group of optimal heat conductance allocations of the hot-, cold- and consumer-side heat exchangers and the intercooler which lead to a maximum dimensionless profit rate. When the total pressure ratio is variable, there exists an optimal total pressure ratio which leads to a double-maximum dimensionless profit rate. Also the exergetic efficiency corresponding to the maximum dimensionless profit rate is obtained.

(3) The effects of total heat exchanger conductance, price ratios and consumer-side temperature on the double-maximum dimensionless profit rate and the corresponding exergetic efficiency, the optimal heat conductance allocations and the optimal total pressure ratio are discussed in detail. One can find that the larger the total heat exchanger conductance and the price ratios, the better the exergoeconomic performance. There exists an optimal consumer-side temperature which leads to a thrice-maximum dimensionless profit rate.

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#### Nomenclature

$a$	price ratio of power output to exergy input rate
$b$	price ratio of thermal exergy output rate to exergy input rate
$C$	heat capacity rate ( $kW / K$ )
$k$	ratio of the specific heats
$T$	temperature ( $K$ )
$U$	heat conductance ( $kW / K$ )
$u_h$	hot-side heat conductance allocation
$u_i$	heat conductance allocation of the intercooler
$u_k$	consumer-side heat conductance allocation
$u_l$	cold-side heat conductance allocation
$u_r$	heat conductance allocation of the regenerator

#### Greek symbols

$\eta$	efficiency
$\Pi$	profit rate ( <i>dollar</i> )
$\pi_1$	intercooling pressure ratio
$\pi$	total pressure ratio
$\tau_1$	ratio of the hot-side heat reservoir temperature to environment temperature
$\tau_2$	ratio of the cold-side heat reservoir temperature to environment temperature
$\tau_3$	ratio of the intercooling fluid temperature to environment temperature
$\tau_4$	ratio of the consumer-side temperature to environment temperature

#### Subscripts

$ex$	Exergy
$H$	hot-side
$I$	intercooler

<i>K</i>	consumer-side
<i>L</i>	cold-side
max	maximum
<i>opt</i>	optimal
<i>R</i>	regenerator
<i>T</i>	total
<i>wf</i>	working fluid
0	Ambient
-	dimensionless

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