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## Enhancement of Desulfurization Process of Gray Cast Iron by using Different Concentrations and Materials

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#### Abstract

This research aims to best of the desulfurisation process through crucible furnace using waste oil motor. The best of desulfurisation process has been studied in crucible furnace of the melting shop with respect to the amount of desulfurising agent, control of carbon, and the temperature as well as the composition and the sulfur content. The results refer to the desulfurisation efficiency of calcium carbide is lower compared to burnt lime. The latter as well as desulfurisation, also has the ability to deoxidize and eliminate of oxygen that has a negative effect on the cast product. In this research, a study of recycling gray cast iron to purity gray cast iron and its effect on mechanical properties. Four kilograms (4.0 Kg) scrap were charged crucible furnace of ten kilograms (10.0 kg) capacity, where furnace using of waste motor oil for scrap heating and melting. The scrap in crucible furnace was heated to a temperature of  $1400 \,^{\circ}$ C and inserted thermocouple to monitor the temperature. For desulphurization, 0.2 kg calcium carbide (CaC<sub>2</sub>) and burnt lime (CaO) were added to the molten in the furnace at 1400  $^{\circ}$ C melt. Then, ladle was used to eliminate of slag on the surface of the molten scrap resulting from desulfurizing agent.

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Keywords: Desulfurisation; Burnt lime; calcium carbide; Scrap; Gray cast iron; Hardness; Strength.

#### 1. Introduction

Sulphur is considered as an undesirable impurity of cast iron because it lowers the mechanical properties and contributes to many defects. The sulphur level in cast iron depends on its level in raw materials, on its removal from the metal before or during cast iron making operation. The present trend is for the user to demand lower sulphur levels while the oil-fired crucible furnace uses waste oil motor of increasing sulphur content. The fluctuations in the sulphur content of oil-fired crucible furnace iron from one cast to another is also a problem that requires some form of sulphur control. For the purpose of lowering the sulphur level in hot metal for steelmaking, it is desirable to study various methods of desulphurization of cast iron outside the blast furnace [1]. Over the past few decades, the demand for grey cast iron worldwide has increased at a rapid rate, along with the increase in the quality of grey cast iron. Grey cast iron producers are required to maximize productivity, reduce production interruptions, and maintain high quality standards while minimizing costs all the time. Modern metallurgy of grey cast iron is directed primarily to improving the quality, effectiveness and competitiveness of its production. One of the main ways for improving the quality of grey cast iron is to reduce its sulphur content. Sulphur is one of the most harmful impurities in grey cast iron recycling process, affecting the internal and surface quality, effect of sulphur on grey cast iron,

- Formation of unwanted sulphides that enhance granular weaknesses and cracks in grey cast iron during solidification.
- It reduces the melting point and inters granular strength.
- Sulphur contributes to the brittleness of grey cast iron. Therefore, acts as stress concentration site in grey cast iron, [2].

There are many researchers who have presented studies on desulfurisation of gray cast iron, such as, Gamal M. El-Kady et al, had investigated the most significant parameters that have a great impact on the desulphurization process in term of energy and efficiency [2]. Annika Yang had studied the basic concepts about the desulphurization process of hot metal in reality [3]. E. T. T Urkdogan and L. J. Mart Onik had studied the utilization of burnt lime in desulfurisation [4]. Frank N. H. Schrama et al., had studied an optimal balance between maximizing sulphur removal capacity and minimizing iron losses [5]. Oyetunji Akinlabi and OMOLE S.O.had investigated desulfurise to from gray cast iron for the purpose of producing ductile iron[6]. In this study is to recycle gray cast iron with crucible furnace that the manner working encourages the pickup of sulfur by an iron molten, and in which it is gray cast iron utilized as scrap. This is because raise sulfur percent (up to about 0.179 %) is present in the scrap after recycling and pick up of sulfur is imminent during with by waste motor oil for melting, so the grey cast iron would treated with desulfurise agent to reduce the sulphur percent to suitable content in cast iron product. The aim of this project is to study the engineering practicality of the following materials for desulfurisation,

- I. Adding calcium carbide (CaC<sub>2</sub>) and burnt lime (CaO) to a grey cast iron melt with oil-fired crucible furnace.
- II. Grey cast iron has become a necessity in the industrialized nations due to its numerous properties, among which are: good castability and low cost of production. Recycling of grey cast iron and desulphurize of grey cast iron scrap by use oil-fired crucible furnace to produce low sulphur grey cast iron will maintain mechanical properties and help small and medium scale enterprises to achieve and sustain industrial growth.

The limitations of the work and the results obtained: Composition control are difficult to control. Also as a result of utilization of waste motor oil as fuel by the furnace used, increase in sulphur pick up in the melt is a sure phenomenon; the charge materials, fuel and product of combustion are all in contact with each other in this system.

#### 2. Desulfurization Technologies

Desulfurisation was analyzed to ensure whether equilibrium is established and to determine the reactions which equilibrate. Desulfurisation can be considered through two successive reactions,

• The sulphur exchange between iron and slag,

$$(S) + [Ca0] \rightleftharpoons [CaS] + 1/2O_2 \tag{1}$$

• The deoxidation reaction which may be one of the following,

 $(C) + 1/20_2 \rightleftharpoons CO \tag{2}$ 

$$(Si) + O_2 \rightleftharpoons SiO_2 \tag{3}$$

$$(Mn) + {}^{1}/{20_{2}} \rightleftharpoons Mn0 \tag{4}$$

$$(Fe) + 1/2O_2 \rightleftharpoons FeO \tag{5}$$

These reactions are in decreasing order of ability to deoxidize and hence, when combined with Equation (2) tend to desulphurize. In desulphurization, the molten cast iron is treated in successive steps by adding highly basic materials such as calcium carbide (CaC<sub>2</sub>), burnt lime (CaO) or soda ash (Na<sub>2</sub>CO<sub>3</sub>) to the molten in especially ladles for removal of oxygen and sulphur (see Table 1). The calcium compounds used for desulphurization are calcium carbide and burnt lime. Calcium carbide is the more common agent. The desulphurization reaction occurs between solid calcium carbide and liquid cast iron at the surface of the

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calcium carbide releasing carbon and producing solid calcium sulphide (CaS). Calcium sulphide has a melting point 2450 °C and specific gravity 2.50. The slag is granular, easily eliminated from the metal surface and does not attack ladle refractories extensively. Table 1 shows the characteristics of various desulphurizing agents.

The reaction is exothermic and results in smaller temperature losses than with other desulphurizer. Only small changes in carbon, silicon and manganese accompany desulphurization. The efficiency of desulphurization depends on the total calcium carbide surface area presented to the liquid iron and the rate of sulphur transport to the surface. The rate of sulphur transport to the surface depends on the sulphur content of the iron. Parameters influencing efficiency are degree of stirring, dwell time, injection rate and calcium carbide particle size [7].

Factor	Calcium carbide CaC <sub>2</sub>	Burnt lime CaO	Soda ash Na <sub>2</sub> CO <sub>3</sub>
Slag produced	Granular- easy to	Granular-easy	Very fluid- complete removal
	remove	to remove	difficult
Fume	Very little	Very little	Appreciable-extraction essential
Temperature	Small- exothermic	Large	Large
loss	reaction		
Silicon loss	Not significant	Not significant	UP to 0.3 %
Storage	To comply with	Keep dry	Keep dry
requirements	statutory regulation		
Refractories	Not important	Preferably basic	

Table 1. The cl	haracteristics	of various	desulphurizing	agents [7]
	laracteristics	of various	desulphulizing	agents, [ / ].

Many techniques are available for stirring (see Figure 1). The shaking ladle provides stirring by vessel movement. The ladle and its contents are supported in framework and subjected to a horizontal gyratory motion that causes efficient mixing of the molten iron and desulphurizing agent, usually  $CaC_2$  and sometimes CaO. The shaking ladle can desulphurize from 2 to 60 tons of iron in a single treatment and useful for preparing base metal in ductile iron production. Other techniques achieve metal slag contact without ladle movement. In mechanical stirring an electrically driven stirring devices, comprising a rotary refractory paddle which is lowered into the ladle to mix the molten iron with a desulphurizing agent. Up to 50 tons of iron can be desulphurize in single treatment. Temperature losses are small and little metal splashing occurs. Other technique use gas (compressed air, N<sub>2</sub> or natural gas) to stir the liquid iron. The porous plug process, nitrogen or compressed air is blown through a porous refractory plug in the ladle bottom, creating turbulence to ensure intimate mixing of the molten metal and the desulphurizing agent usually calcium carbide. This method is particularly suitable for small foundries, mainly for ductile iron production. Up to 10 tons of iron can be treated at low cost. Injection technique. The desulphurizing is metered into a gas flow by powder dispenser and injected through a refractory lance immersed in the molten iron. This method is used in the USA for ductile iron production and for reducing the sulphur content of grey, but other processes are generally preferred because the lances require frequent maintenance and injection blockage problems can arise. Direct tapping technique, the desulphurizing agent is placed in the ladle bottom and molten iron tapped on to the agent. Up to 50 % of the sulphur can be removed by this method, although results are not always reproducible. Only the use of Na<sub>2</sub>CO<sub>3</sub> will produce a very significant decrease in sulphur content, Na<sub>2</sub>CO<sub>3</sub> does, however produce a very fluid slag which must be coagulated and removed. Unless great care is taken, soda ash slag defects can arise in the casting [8].

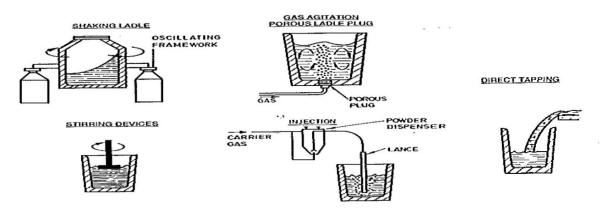


Figure 1. Techniques of ladle desulphurization, [8].

#### **3. Experimental Work**

#### 3.1 Materials

Materials used in this work are: gray cast iron cylinder automobile engine was used as scrap, calcium carbide (CaC<sub>2</sub>) and burnt lime (CaO) used as desulphuriser.

#### 3.2 Equipment

- Crucible furnace (ten kilograms) capacity for melting the scrap.
- Waste motor oil was used for heating.
- Thermocouple with temperature controller to monitor the temperature, as shown.
- Spectrometer was used for inspection the chemical analyses.
- Wooden cylindrical pattern of diameter 20 mm by 200 mm length was used to prepare sand mould made of silica sand.
- The sand mould used was prepared by adding (5% bentonite) as a binder and (5% water) into silica sand according to [9]. The mould was prepared using sand round the pattern, to create a cavity upon which the molten metal was poured after the withdrawn of pattern from the sand.

#### 3.3 Methods

The following are the techniques used in carrying out the research study,

I. Chemical Analysis, The sample scrap was analyzed using spectrometer to determine a chemical composition of the elements present in them. Spark test was performed on each sample at the head and at the middle point, and reading was taken and recorded as shown in Table 2.

Elements	С	Si	Mn	Р	S	Fe
% Compositions	3.79	1.82	0.63	0.12	0.037	Balance

Table 2. Composition of sample scrap.

II. Melting and Casting, Pieces with size of (6-12 cm) scrap was putted in the crucible. Four kilograms (4.0 Kg) scrap were charged crucible furnace of ten kilograms (10.0 kg) capacity, where furnace using of waste motor oil for scrap heating and melting. The scrap in the oil-fired crucible furnace was heated to a temperature of 1400 °C and inserted thermocouple with temperature controller to monitor the temperature. For desulphurization, 0.2 kg calcium carbide ( $CaC_2$ ) and burnt lime (CaO) were added to the molten in the furnace at 1400 °C melt. Then, ladle was used to eliminate of slag on the surface of the molten scrap resulting from desulfurizing agent. Thereafter, the treated molten was poured into the prepared mould immediately after the completion of the two treatments at a temperature higher than 1350°C to ensure the removal of gaseous cavities,. As shown in table 3 in details distinguish of all additives that were used in this study, Figure 2.



Figure 2. Standard test sample.

Table 3.	Theoretical	charge ca	lculation.
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No	Charge (Kg)	CaO% of charge weight	CaC <sub>2</sub> % of charge weight
А	4	-	-
В	4	-	5
С	4	5	-

- III. Samples Preparations, The sample scrap and the sample product were prepared for mechanical, chemical analysis, [10-25]. The mechanical tests were done to inspect the tensile, impact and Brinell hardness properties of the samples. Samples were machined using lathe and milling machine.
- IV. Tensile inspection, tensile specimen was machined using lathe machine, according to universal tester specification of (50 mm) gauge length which fits into testing machine. The tensile test specimen shown in Figure 3 was fixed on the universal testing machine at the jaws one end immovable and the other movable. The machine was then operated, which pulled at constant rate of extension and the tensile test performed in accordance with ASTM E8/E8M-13a standards [26]. The tensile test was performed at room temperature and a cross-head speed of 2 mm/min. where, a three samples test for each sample types were used to calculated the tensile properties, [27-42].

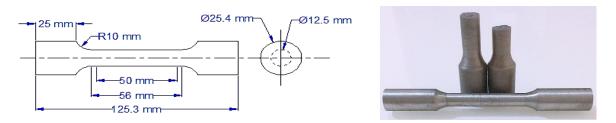


Figure 3. A standard tensile sample.

V. Impact inspection, Charpy impact inspection was performed with notched specimen performed in accordance with ASTM E23, according to the research Tanzim Nasir [43]. The impact test specimen shown in Figure 4, so, three samples were used for each test, and then using the average value to calculate the impact characterizations, [44-57].

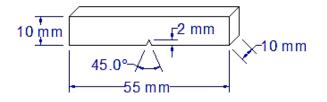




Figure 4. A standard Charpy impact specimen.

VI. Hardness inspection, Brinell hardness specimens were machined using milling machine from the scrap and the product. Samples were performed in accordance with ASTM E10 standards that conform to specification which fits into digital Brinell hardness inspector machine. The surface of the entire hardness inspect specimen was grinded using 200,400 and 1200 SiO<sub>2</sub> emery papers to make them flat and smooth, which using a three sample for each test to evaluate the average value for hardness properties for each sample types, [58-72].

#### 4. Results and discussion

The tensile analysis was shown in Table 4 of sample scrap and sample product A, B, C respectively. The tensile, elongation, impact and hardness values are as presented in Table 4. The result of the composition analysis was as presented in Table 5. The product from melt and casting was satisfactory good with no defect.

Sample	UTS (MPa)	BHN	Impact (J)
А	248	400.3	5.66
В	236	372.6	5.37
С	248	387.6	5.95

Table 5. The composition analysis of samples.

Table 4. Tensile analysis, impact and hardness values of scrap and sample (G).

Sample	Chemical Properties								
	С%	Si%	Mn%	P%	S%	Ni%	Mo%	Cr%	Fe%
А	5.22	1.73	0.19	0.060	0.179	0.026	0.002	0.027	Bal.
В	5.22	2.07	0.19	0.047	0.112	0.024	0.013	0.023	Bal.
С	4.07	1.38	0.77	0.052	0.054	0.027	0.005	0.029	Bal.

#### 4.1 Composition analysis and desulphurization

The result obtained from the composition of the used scrap analyzed in Table 5 indicated that C% of 3.97% was increased to 5.22 %, 5.22 % and 4.07 % in samples A, B and C respectively (see Table 5), this represents a total carbon raise of 26.0 %, 31.0% and 1.0% in samples A, B and C respectively. Although the oxidation was due to the nature of the mode of operation of crucible furnace, in which the fuel, charges and the products of combustion are all in contact with themselves. This was supposed to cause a loss of carbon, but carbon percent gained exceeds carbon percent loss due to the melting method. As a result, there was such a large increase in samples A and B.

In sample C, due to the treated of the molten by added a desulphurizer agent (5%CaO) of scrap weight, whereby amount of the carbon is lost by its react with oxygen and released carbon dioxide. In contrast to, a desulphurizer agent (5%CaC<sub>2</sub>) of scrap weight was added in sample B, the carbon remained in the molten and is not released as gas or slag, so the carbon percent was larded. As a result of the low purity of the scrap used and the processing method in the oil-fired crucible furnace high sulphur content up to 0.1 % was still found in the casting. In sample B, treated of the molten by added a desulphurizer agent (5% CaC<sub>2</sub>) of scrap weight, S% of the used scrap (0.179%) was decreased to 0.112 %. This S% dropped was very little, not within the specified range that guarantees better mechanical properties to gray cast iron.while, in sample C was added a desulphurizer agent (5%CaO) of scrap weight, S% of the used scrap (0.179%) was decreased to 0.054 %.

#### 4.2 Tensile strength

The results were obtained in Table 4 from tensile analysis showed the ultimate tensile strength obtained for sample A was 248MPa and sulphur percent 0.179% without added a desulphurizer agent, sample B was 236MPa and sulphur percent 0.112% with added ( $5\%CaC_2$ ) while for sample C was 248MPa and sulphur percent 0.054% with added (5%CaO) which is significantly alright. The ultimate tensile strength obtained for sample C was 248MPa while for sample B is 236MPa which is significantly alright.

#### 4.3 Brinell hardness

The average hardness obtained in sample A was 400.3 HB, in sample B was 372.6 HB and in sample C was 387.6 HB as shown in Table 4.

#### 5. Conclusions

Treated of the molten by added a desulphurizer agent  $(5\%CaC_2)$  and (5%CaO) were carried out on grey cast iron. The resulting hardness and tensile was investigated.

The results show that:

1. Burnt lime (CaO) as a desulphurizer in sample B

Burnt lime has been found to be capable of removing sulphur from grey cast iron; the desulphurization proceeds at a high rate. The sulphur level in a grey cast iron molten depends on initial sulphur and type melting furnace. At crucible furnace that the mode of firing encourages the pickup of sulphur by the metal, and in which it is grey cast iron utilized as scrap. This is because high sulphur (up to about 0.179 %) is present in the scrap after recycling and pick up of sulphur is imminent in the course of using waste motor oil for melting, so grey cast iron recycling would have undergone desulphurization with(CaO) to reduce the sulphur content to appropriate level(0.054% S) in the cast product C.

2. Calsium carbide (CaC<sub>2</sub>) as a desulphurizer in sample B

Calcium carbide was found that it desulfurizer is inappropriate for cast iron that contains a high carbon percent in it as a result of increasing the percentage of carbon to more than 5% due to the liberation of carbon as a result of the following reaction  $(CaC_2(s) + \underline{S} \leftrightarrow CaS(s) + 2\underline{C})$ , where the carbon remains in the molten according to Annika Yang [7]. Also, sulphur percent removal in a sample B very low model was 0.112% S.

3. Improved ultimate tensile strength (248 MPa) and impact (5.95 J) in sample C after treated molten with (CaO).

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